

Hydrogen Production

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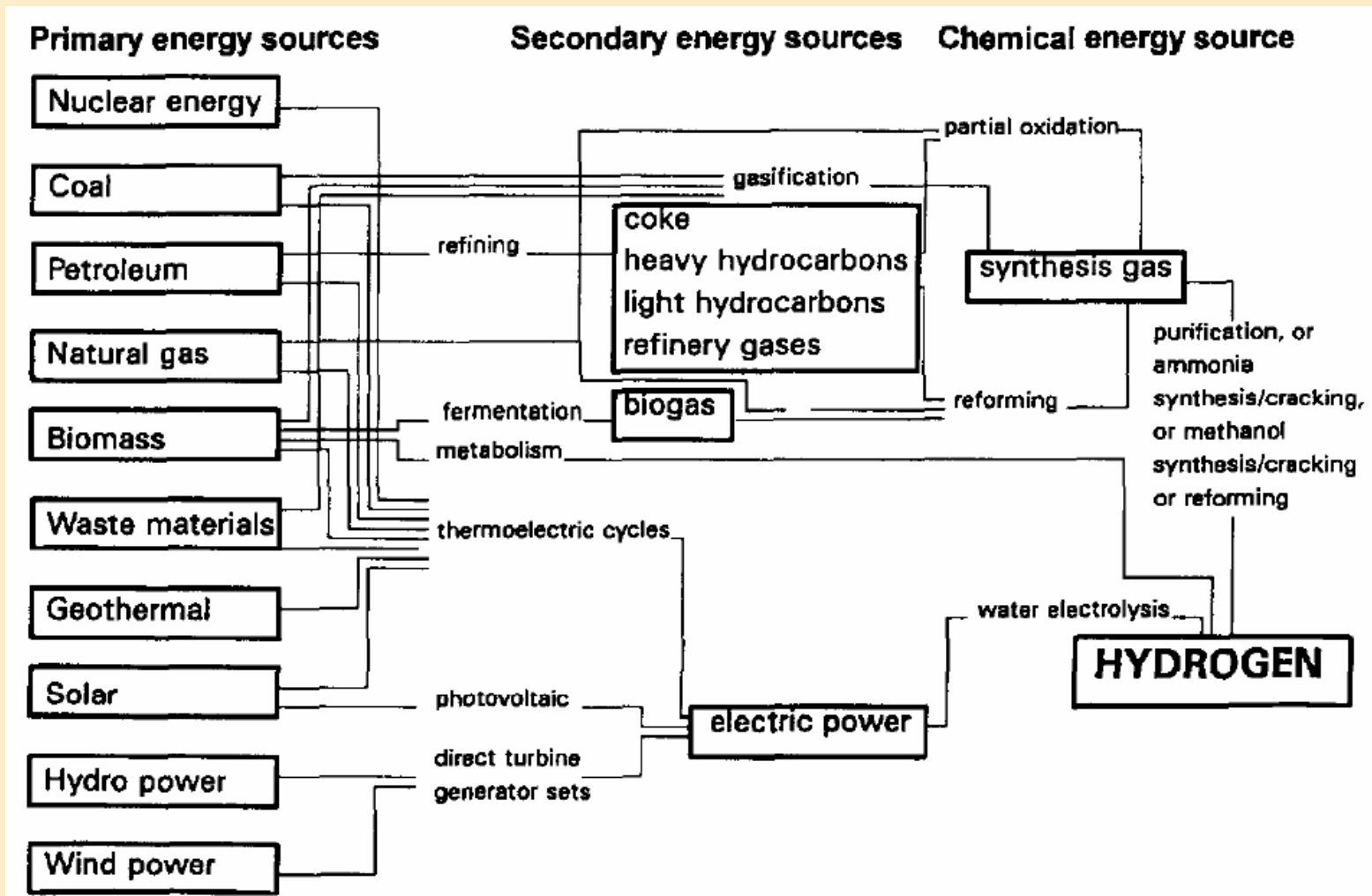
Neutrons for the Hydrogen Economy
ANSTO
22 June 2007

www.uq.edu.au



THE UNIVERSITY
OF QUEENSLAND
AUSTRALIA

Production of hydrogen



Summary

- Hydrogen from water
 - Electrolysis
 - Photocatalysis
 - Biological catalysis
 - Thermal decomposition
 - Chemical cycles
- Hydrogen from hydrocarbons
 - Anaerobic pyrolysis/thermal cracking
 - Gasification
 - Steam reforming



Hydrogen from water

Electrolysis – redox reaction

- Water is oxidized at the anode.
$$2\text{H}_2\text{O} \rightarrow \text{O}_2 + 4\text{H}^+ + 4\text{e}^-$$
- Water is reduced at the cathode.
$$4\text{H}_2\text{O} + 4\text{e}^- \rightarrow 2\text{H}_2 + 4\text{OH}^-$$

Most recent commercial electrolyzers use a PEM membrane (formerly alkali cells), low current density means higher efficiency but at higher cost. Efficiencies of 60—70% are routinely achieved at reasonable cost. DOE target for 2010 is 75%. New low-cost nanomaterials electrodes by Quantum Sphere have achieved 75% at 300 mA/cm².



Hydrogen from water

Photocatalysis

Fujishima & Honda 1972

Titania (anatase) is the most widely studied semiconductor because it is inert, stable, and has redox potential is within its bandgap range:

Electronic absorption edge occurs in the UV (3.2 eV or 400 nm).

Many studies seek to improve band gap by doping (e.g. with oxides or but efficiency remains low (below 10%) and there are many materials inconsistencies

UNSW have characterised TiO_2 finding defects (Ti and O vacancies), and believe materials can be improved by tailoring the defect properties

ANSTO looking at functionalising the surface of TiO_2

.....



Hydrogen from water

Photocatalysis

Other materials can be used:

ZnO (E_g 3.2 eV)

ZnS (E_g 3.6 eV)

Fe₂O₃ (E_g 3.1 eV)

WO₃ (E_g 2.8 eV)

SiTiO₃ (E_g 3.2 eV)

New materials needed – mesoporous transition metal oxides, composites with nano-crystalline semiconductors within the pores of host structures, that can be further modified through ion implantation



Hydrogen from water

Biological catalysis of water splitting by enzymes

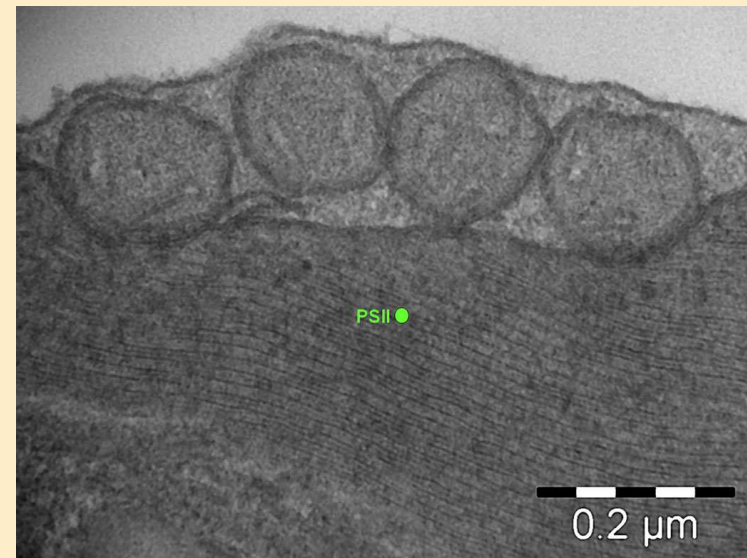
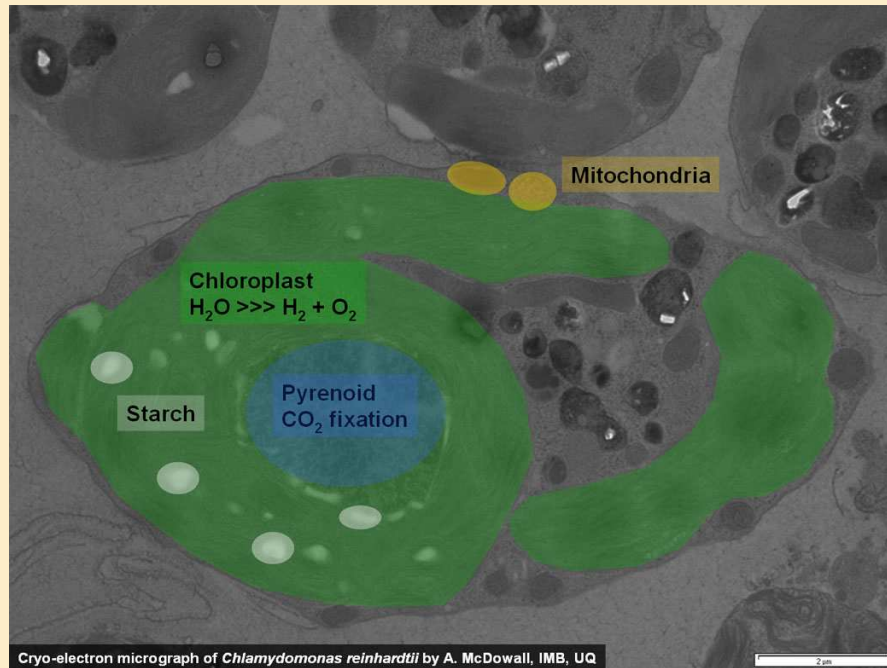
A three step process:

1. Photosystem II
 $2\text{H}_2\text{O} = 4\text{H}^+ + 4\text{e}^- + \text{O}_2$ (aerobic phase, atmospheric oxygen)
2. $\text{H}^+ + \text{e}^-$ is stored by reaction with CO_2 as starch through photosynthesis
3. Starch is decomposed by hydrogenase to hydrogen under anaerobic conditions

Present work is on modification of green algae, e.g. *Chlamydomonas*



Hydrogen from water



Hydrogen from water

Thermal decomposition

Above about 1800 K, water (steam) begins to dissociate into a mixture of H₂, O₂, H₂O, O, H and OH. The extent of dissociation increases with increasing temperature and decreasing pressure. The water and the diatomic hydrogen and oxygen species completely dissociate into atomic H and O above about 3500 K under equilibrium conditions at 1 mm Hg absolute pressure.

Separation of H₂ and O₂ is the main problem in addition to achieving high temperature.

Quenching proposed by CNRS 1986

Use of glow discharge and ceramic dissociator nozzle investigated by Pyle et al 1998

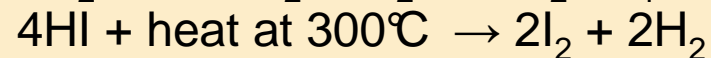
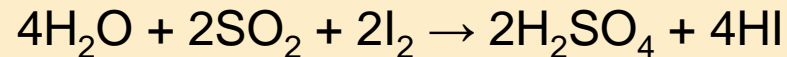
So far only low efficiencies (up to 2%) have been achieved



Hydrogen from water

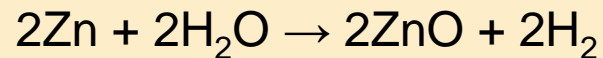
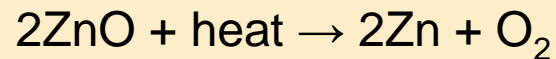
Water-splitting using chemical cycles

Sulphur-iodine cycle



Presents engineering challenges

Metal/metal oxide cycle, e.g. at 1900°C

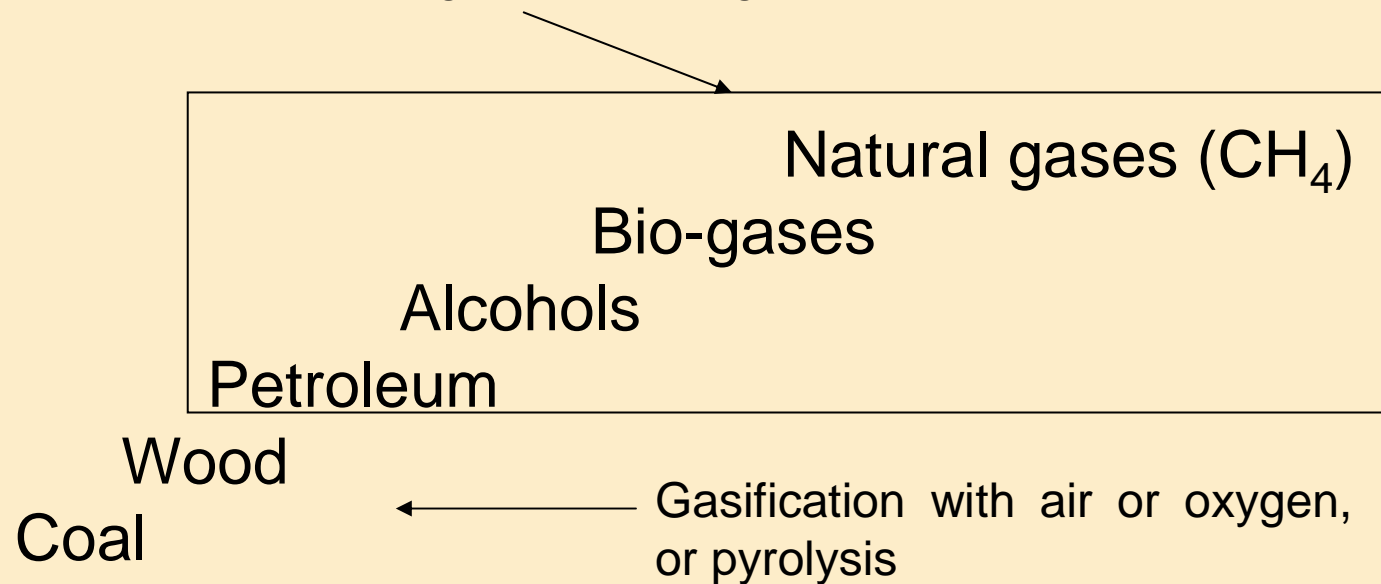


Challenge is to find stable materials that operate at lower temperatures



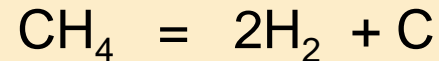
Hydrogen from hydrocarbons

Pyrolysis, Partial oxidation, or chemical processing:
Steam reforming, cat. cracking, POX, CPO



Hydrogen from hydrocarbons

Pyrolysis



In principle a simple process but a major engineering challenge – high temperature and C removal.

Kaverner CB&H process uses a plasma torch to pyrolyse feed. Plasma gas is recirculated H_2 . Process commercial since 1999.

Cost of CB&H process is comparable with steam reforming without CO_2 capture and sequestration

Catalysts required to reduce temp.

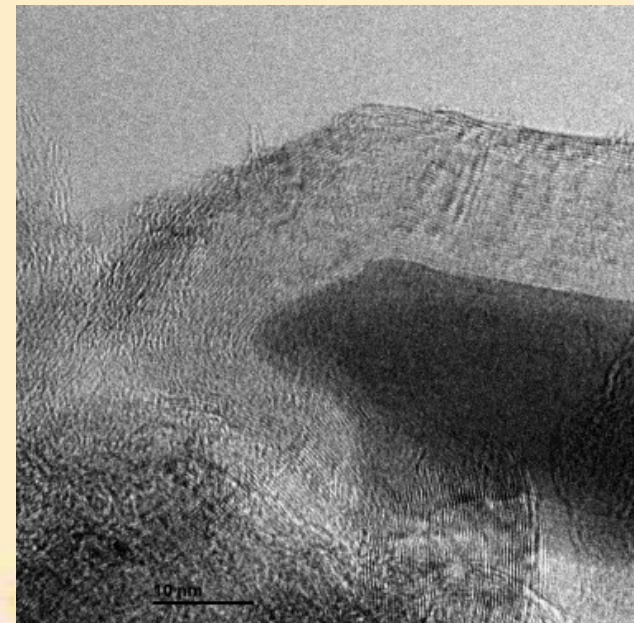
Carbon encapsulates catalyst particles

Decomposition of higher hydrocarbons yields secondary products

TEM of Fe (10 wt.%)/AC-lignite

after CH_4 pyrolysis in absence of O_2

N Murador et al *Catalysis Today*, 116(3), 281



Hydrogen from hydrocarbons

Gasification

A wide variety of processes for heavy liquid petroleum feeds through to coal and biomass

Oxygen-blown or air-blown gasifiers

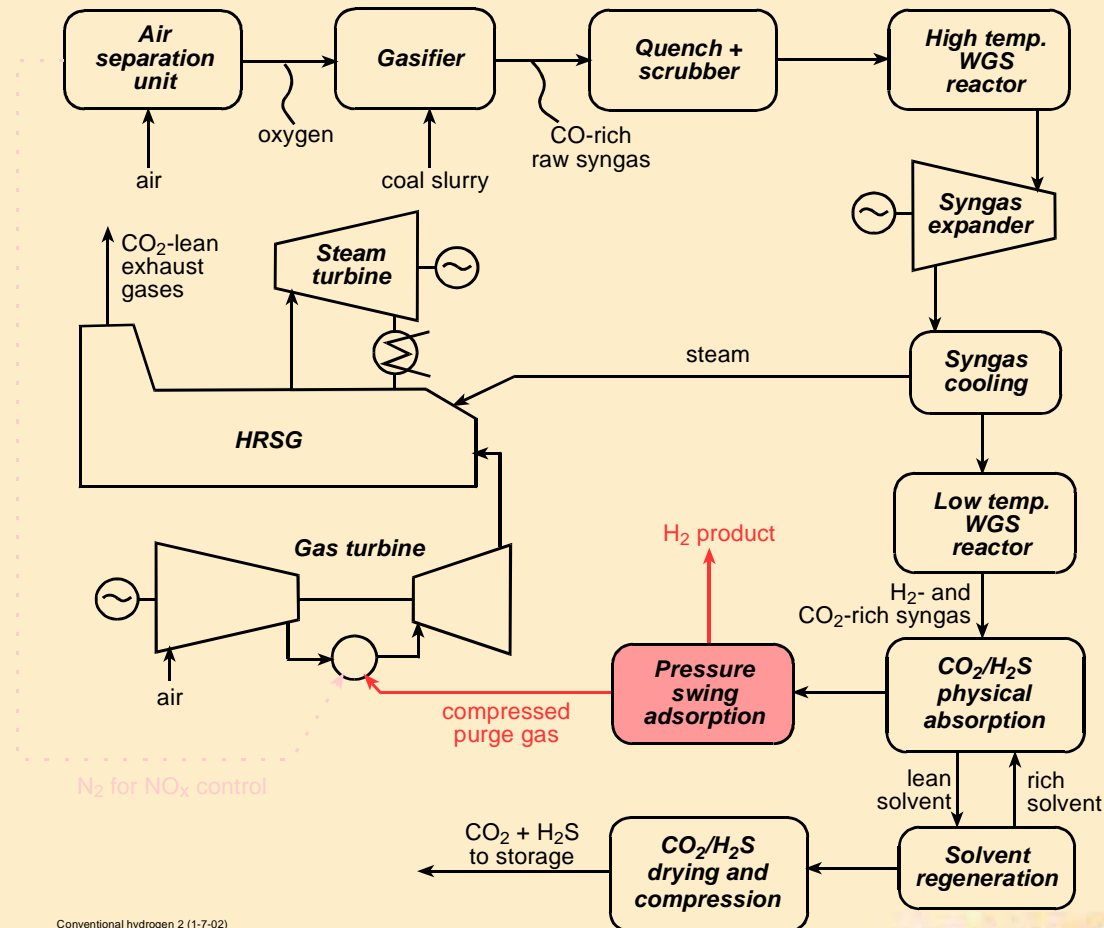
Fluid bed, entrained bed, or moving bed reactors can be used

Downstream processing required to purify the H₂ and capture CO₂

Products depend on operating conditions and feedstock



Conventional Gasification Technology for H₂ Production with CO₂ Capture



Conventional hydrogen 2 (1-7-02)

Hydrogen from hydrocarbons

Coal gasifier product gases

| | BG-Lurgi gasifier (non-slugging) | BG-Lurgi slagging gasifier | Moving bed O ₂ -blown (Lurgi) | Fluidised bed (Winkler) | Entrained bed O ₂ blown (Texaco) | Entrained bed air-blown | Entrained bed O ₂ blown (Shell) |
|-------------------------------|-------------------------------------|-------------------------------|--|----------------------------|---|----------------------------|--|
| Coal | Pittsburg 8 | Pittsburg 8 | Illinois no.6 | Texas Lignite | Illinois no.6 | Illinois no.6 | Illinois no.6 |
| Ar | trace | Trace | trace | | 0.9 | trace | 1.1 |
| CH ₄ | 8.5 | 7.2 | 3.3 | 0.7 | 0.1 | 1.0 | 26.7 |
| C ₂ H ₆ | 0.7 | 0.1 | 0.1 | 4.6 | 30.3 | 9.0 | 63.1 |
| C ₂ H ₄ | 0.3 | 0.2 | 0.2 | 28.3 | 39.6 | 16 | 1.5 |
| H ₂ | 29.1 | 39.0 | 21.0 | 33.1 | 10.8 | 6 | 4.1 |
| CO | 18.0 | 55.5 | 5.8 | 15.5 | 0.7 | 62 | 2.0 |
| CO ₂ | 31.1 | 3.9 | 11.8 | 0.6 | 0.1 | 5.0 | 1.3 |
| N ₂ | 2.4 | 4.0 | 0.2 | 0.1 | 16.5 | 100.0 | 100.0 |
| NH ₄ | 100.0 | 100.0 | 0.4 | 16.8 | 1.0 | | |
| H ₂ O | | | 61.8 | 0.2 | 100.0 | | |
| H ₂ S | | | 0.5 | 100.0 | | | |
| Total | | | 100.0 | | | | |

From: Larminie and Dicks, *Fuel Cell Systems Explained*, Wiley 2004



Hydrogen from hydrocarbons

Catalytic steam reforming

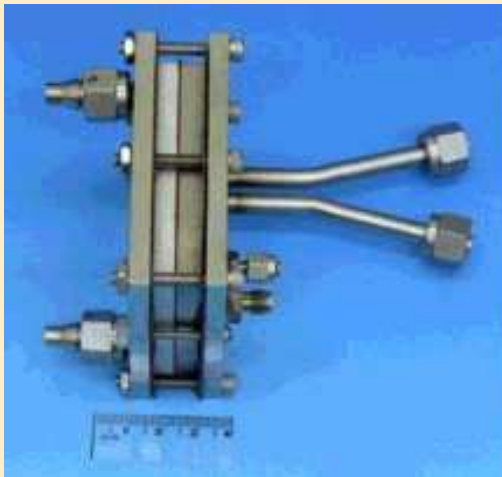


Steam Reforming $\text{CH}_4 + \text{H}_2\text{O} \rightleftharpoons \text{CO} + 3\text{H}_2$ $\Delta H = +205.9 \text{ kJ/mol}$ [1]
(higher hydrocarbons generally react at lower temperatures and are less endothermic)

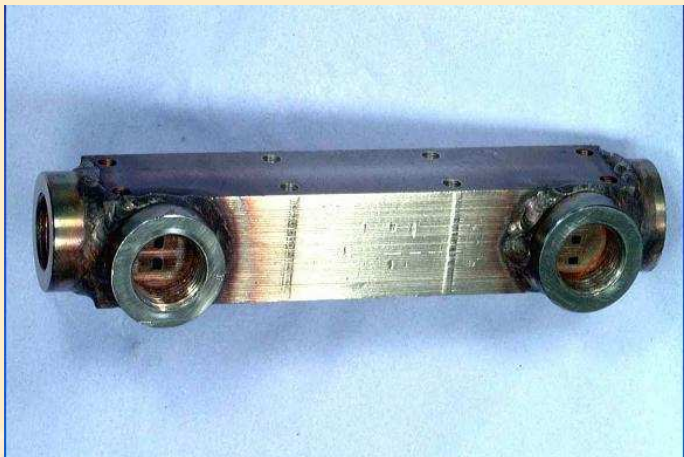
Water Gas Shift $\text{CO} + \text{H}_2\text{O} \rightleftharpoons \text{CO}_2 + \text{H}_2$ $\Delta H = -41.1 \text{ kJ/mol}$ [2]

Hydrogen from hydrocarbons

steam reforming at the small scale



Batelle, Northwest
National Laboratory
Gasoline reformer



Advantica technologies
Natural gas reformer

National Hydrogen Materials Alliance

RSVP: Wednesday, 11 October 2006
Sam East CSIRO 02 4969 2189



- A cluster of 11 universities and ANSTO
- Budget ca. \$10 million 2005-8
- R&D devoted to materials development
 - Production
 - Storage
 - Utilisation (fuel cells)

NATIONAL RESEARCH
FLAGSHIPS



Hydrogen Generation and End Use projects:

- *New catalyst materials for hydrogen generation from hydrocarbon fuels*
- *Integration of electrolysis systems*
- *Photocatalytic materials for hydrogen production by water splitting*
- *Materials for advanced hydrogen fuel cells*

Hydrogen Storage projects:

- *Storage materials based on lithium*
- *Storage materials based on magnesium*
- *Storage in carbons*
- *Storage in porous materials*



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Brisbane, Queensland
15 - 19 June 2008

www.whec2008.com

